AMENDMENTS TO THE CLAIMS:

Claim 1 (currently amended) A process for the preparation of cross linked enzyme crystals of hydrolases, and oxidoreductases which are solvent tolerant, thermostable and shear resistant, the process comprising the steps of :

- (a) crystallizing—the enzymes an enzyme in aqueous buffer with a suitable salts and cosolvents a co-solvent in the presence of surfactants at a temperature ranging between from about 4° to about 10° C for a period ranging between from about 5 hr. to about 15 days to obtain the enzyme crystals of the protein having a particle size ranging between from about 50 to about 150 microns;
- (b) reacting the <u>enzyme</u> crystals of the enzyme obtained in step (a) with a multifunctional crosslinking agent in the presence of buffer of pH ranging between 3–8 from about 3 to about 8 at a temperature ranging between from about 4° to about 25° C to get the crossed linked enzyme erystal crystals;
- (c) washing the cross linked crystals with a reagent that is capable of removing the excess of the said multifunctional cross linking reagent agent so as to obtain the washed cross linked protein crystals; and
- (d) coating the cross linked protein crystals with a suitable surfactant, and lyophilizing it the protein crystals to obtain the a stable product.
- 2. (currently amended) The process as claimed in claim 1, wherein said enzymes the enzyme is selected from the group consisting of hydrolases and the said enzyme is comprises a starch hydrolyzing amylase namely glucoamylase.
- 3. (currently amended) A process as claimed in claim 1, wherein said oxidoreductase enzyme is comprises a plant peroxidase.
- 4. (currently amended) The process as claimed in claims 1 to 3 wherein said oxidase oxidoreductase is selected from the group of plant peroxidases consisting of Horse radish, Ipomea or Saccharum peroxidases.

- 5. (currently amended) A process as clamed in claim 1 wherein the crystallizing salt is comprises a salt selected from the group consisting of sulphate of ammonium or and sulphate of sodium either as saturated solution or crystals.
- 6. (currently amended) A process as claimed in claim ± 2 wherein the said buffer used for the cross linked glucoamylase preparation is an aqueous buffer of 10mM -0.5M of acetate having a pH of <u>about</u> 4.5.
- 7. (currently amended) A process as claimed in claim ± 3 wherein the said buffer used for the cross linked peroxidase preparation is an aqueous buffer of 10mM -0.5M phosphate or tris having a pH of about 6.5-8.0.
- 8. (currently amended) A process for the preparation of the cross linked protein enzyme erystal crystals as claimed in claim 1, wherein the said co-solvent is an alcohol having a concentration of about 1 to about 20% 1-20%, example selected from the group consisting of 2-methyl,2,4 pentane diol; 2-methyl-2,4-pentane diol, 2-propanol; 1,5 pentane diol, ethanol, and isoamyl alcohol.
- 9. (currently amended) A process as claimed in <u>claim claims</u> 1 to 8, wherein said crystal is a <u>microcrystal crystals</u> are <u>microcrystals</u> of <u>about</u> 150 microns or less.
- 10. (currently amended) A process as claimed in claim 1, wherein the cross linking reagents used is agent comprises glutaraldehyde, and starch dialdehyde.
- 11. (currently amended) A process as claimed in claim 1, wherein the said surfactant used is is selected from the group consisting of anionic, non-ionic, or and cationic surfactants.
- 12. (currently amended) A process as claimed in <u>claim claims 1 to 11</u> wherein the <u>cationic</u> surfactant <u>comprises a cationic surfactant selected from the group consisting of used is</u> cetyl trimethyl ammonium bromide <u>or and</u> cetrimide.

- 13. (currently amended) A process as claimed in <u>claim 11</u> claims 1-12 wherein the anionic surfactant <u>used is is an anionic surfactant comprising</u> dioctylsulfosuccinate Aerosol OT.
- 14. (currently amended) A process as claimed in claims 1 to 13 claim 11 wherein the non-ionic surfactant used is selected from the group consisting of alkyl phenol ethoxylate, sorbitan trioleate, sorbitan tristerate. Examples Tween 20, Tween 80 and Triton X-100.
- 15. (currently amended) A process as claimed in <u>claim 1</u> <u>claims 1 to 14</u> wherein the said surfactant provides a weight ratio of <u>crosslinked enzyme cross linked protein</u> crystals to surfactant between about 1:1, and about 1:5, <u>preferably between about 1:1 and about 1:2</u> and is in a lyophilized form.
- 16. (currently amended) The process as claimed in claim 2 +, wherein the cross linked gulcoamylase is active in a + 1:1 mixture of water organic solvents n-dodecane; n-hexane; chloroform; and dimethyl sulphoxide.
- 17. (currently amended) A process as claimed in <u>claim 1</u> any of the preceding claims, wherein the said <u>crosslinked cross linked</u> enzyme <u>crystal is having crystals have</u> resistance to exogenous proteolysis, such that said <u>crosslinked cross linked enzyme crystal retains crystals retain</u> at least 91% of <u>its their</u> initial activity after incubation for three hours in the presence of a concentration of Protease that causes the soluble uncrosslinked form of the enzyme that is crystallized to form said enzyme <u>crystal that is crystals that are crosslinked</u> to lose at least 94% of <u>its their</u> initial activity under the same conditions, wherein said <u>crystals are crystal is</u> in lyophilized form.
- 18. (currently amended) The process as claimed in claim <u>3</u> +, wherein the cross linked Peroxidases are active in organic solvents like selected from the group consisting of toluene; 80% dioxane, chloroform; 2-propanol; chloroform; acetone; ethanol; acetonitrile; methnol; and dioxane.

- 19. (currently amended) A process of continuous generation of glucose solution making use of the cross linked enzyme <u>crystal</u> <u>crystals</u> as claimed in <u>claim 2 elaims 1 to 18</u>, wherein the said cross linked glucoamylase crystals are packed in a jacketed column for the continuous saccharification of starch solution having a concentration of <u>about 1 to about 20 1–20</u>% <u>preferably 4–10%</u> (W/V) at <u>a pH of about 4.5</u> and at <u>about 60° C</u> with a yield of <u>about 110g</u> glucose /L/hour at a residence time of <u>about 7.6</u> min.
- 20. (currently amended) A process of continuous generation of glucose solution making <u>use</u> of the cross linked glucoamylase <u>crystals</u> as claimed in claim 19, wherein the said enzyme <u>crystals</u> can also act upon a solution of <u>about 1 to about 30 % 1–30</u>%(W/V) of maltodextrin of DE 10-15 <u>preferably 10% (W/V) maltodextrin with a DE of 10–14</u> at a pH of <u>about 4.5</u>, at <u>about 60° C</u> thereby producing <u>a</u> glucose solution within <u>about 1-8</u> min with a yield of <u>about 463</u> to <u>about 714</u> g/L/h.
- 21. (currently amended) A process as claimed in <u>claim 4 claims 1 to 18</u> wherein the crystals of plant peroxidase <u>especially comprising</u> Horse radish peroxidase <u>produce 2,4-dimethyl produces</u> 2,4 <u>dimethyl phenol dimer dimmer</u> from monomer dissolved either in 2-propanol or toluene and the catalysis <u>is</u> carried out at <u>about 50° C for about 30 min.</u> in the presence of <u>about 30%H₂O₂.</u>
- 22. (new) A process as claimed in claim 1 wherein the said surfactant provides a weight ratio of cross linked protein crystals to surfactant between about 1:1 and about 1:2 and is in a lyophilized form.
- 23. (new) A process of continuous generation of glucose solution making use of the cross linked enzyme crystals as claimed in claim 2, wherein the said cross linked glucoamylase crystals are packed in a jacketed column for the continuous saccharification of starch solution having a concentration of about 4 to about 10% (W/V) at a pH of about 4.5 and at about 60° C with a yield of about 110g glucose/L/hour at a residence time of about 7.6 min.

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24. (new) A process of continuous generation of glucose solution making use of the cross linked glucoamylase crystals as claimed in claim 19, wherein the said enzyme crystals act upon a solution of about 10%(W/V) of maltodextrin of DE 10-14 at a pH of about 4.5, at about 60° C thereby producing a glucose solution within about 1 to about 8 min with a yield of about 463 to about 714 g/L/h.